Technical Note: Drifting versus anchored flux chambers for measuring greenhouse gas emissions from running waters

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Abstract

Stream networks were recently discovered as major but poorly constrained natural greenhouse gas (GHG) sources. A fundamental problem is that several measurement approaches have been used without cross comparisons. Flux chambers represent a potentially powerful methodological approach if robust and reliable ways to use chambers on running water can be defined. Here we compare the use of anchored and freely drifting chambers on various streams having different flow velocities. The study clearly shows that (1) anchored chambers enhance turbulence under the chambers and thus elevate fluxes, (2) drifting chambers have a very small impact on the water turbulence under the chamber and thus generate more reliable fluxes, (3) the bias of the anchored chambers greatly depends on chamber design and sampling conditions, and (4) there is a promising method to reduce the bias from anchored chambers by using a flexible plastic foil seal to the water surface rather than having rigid chamber walls penetrating into the water. Altogether, these results provide novel guidance on how to apply flux chambers in running water, which will have important consequences for measurements to constrain the global GHG balances.

1 Introduction

Rivers and streams have been identified as important links in the global carbon cycle. They receive and transport terrestrial carbon from the land to the ocean and are also shown to be a net source of greenhouse gases (GHG), i.e carbon dioxide (CO_2) and methane (CH_4) (Aufdenkampe et al., 2011;Battin et al., 2008;Cole et al., 2007;Tranvik et al., 2009). In a recent study, the global CO_2 emissions from rivers and streams were estimated to be 1.8±0.25 Gt C $year^{-1}$ (Raymond et al., 2013), which corresponds to 70% of the global ocean carbon sink (Le Quéré et al., 2014). Due to the lack of knowledge of surface area and gas exchange velocity, the smallest streams are considered as a major unknown component of regional to global scale GHG emission estimates (Bastviken et al., 2011;Cole et al., 2007). Despite these knowledge gaps, there are strong indications that small streams have the highest gas exchange velocities (Aufdenkampe et al., 2011), highest CO_2 partial pressures (Koprivnjak et al., 2010) and cover the largest fractional surface area within fluvial networks (Butman and Raymond, 2011). A continental-scale analysis of CO_2 efflux from streams and rivers revealed a continuous decline of the fluxes with increasing size and discharge of the aquatic systems (Hotchkiss et al., 2015).

Ecosystem-scale fluxes of CO_2 and CH_4 from running waters are often derived indirectly using measured gas partial pressure in the surface water in combination with estimates of a gas exchange velocity. For sparingly soluble gases, the exchange velocity is mainly controlled by turbulence at the water-side of the air-water interface. In smaller rivers and streams, turbulence is driven by stream velocity, depth and bottom roughness (Marion et al., 2014), and the resulting gas exchange velocities are often parameterized with one or more of the following terms: stream order, slope, flow velocity, discharge, width and depth (Alin et al., 2011;Raymond et al., 2012;Wallin et al., 2011). In small streams, reach-scale estimates of the gas exchange velocity can also be derived from gas tracer experiments, whereby a volatile

tracer (e.g., propane or sulfur hexafluoride) is injected upstream and the longitudinal decrease of its dissolved concentration is measured (Halbedel and Koschorreck, 2013;Raymond et al., 2012). For practical reasons, tracer gas injections are limited to application in small streams and alternative methods suitable for a greater range of stream sizes are needed. Moreover, recent studies revealed that the gas exchange velocity of CH_4 can be enhanced by microbubbles (Beaulieu et al., 2012) and can therefor differ from that of the volatile tracer. To better constrain ecosystem-scale estimates of GHG emissions and to improve the understanding of the flux drivers in small running waters, reliable methods are required that allow direct measurements.

As eddy-covariance (Baldocchi, 2014) measurements are not suitable for small streams, gas flux chambers that float on the water surface are a straightforward and inexpensive method for direct measurements of gas fluxes, and can easily be replicated over time and space (Bastviken et al., 2015). The gas flux is determined from the change of the gas concentration in the chamber headspace over time. Floating chambers have been frequently applied for measuring gas fluxes in large rivers, reservoirs and lakes (e.g., Beaulieu et al., 2014;DelSontro et al., 2011;Eugster et al., 2011).

Chamber measurements have been criticized because submerged chamber edges are thought to disrupt the aquatic boundary layer, thereby affecting the gas exchange (Kremer et al., 2003). Comparisons of floating chambers with other flux measurement techniques were performed in lakes, rivers and estuaries. While some studies have reported a tendency of floating chambers to yield higher fluxes than other methods (Raymond and Cole, 2001;Teodoru et al., 2015), others found reasonable agreement (Gålfalk et al., 2013;Cole et al., 2010).

In streams and rivers, floating chambers have been deployed anchored at one spot (anchored chambers) (Sand-Jensen and Staehr, 2012;Crawford et al., 2013), or freely drifting with the water (drifting chambers) (Alin et al., 2011;Beaulieu et al., 2012). Although based on the

same principle, the two deployment modes have fundamental differences. Because of the higher velocity difference between the chamber and the surface water, anchored chambers in running waters may create additional turbulence around the chamber edges (Kremer et al., 2003). If the effect of this turbulence on fluxes is minor, anchored chambers would be advantageous as the area covered by the chamber can be controlled and because practical work with anchored chambers is relatively simple. Drifting chambers will likely induce less turbulence in the surface water, however it is difficult to control their coverage, potentially resulting in spatially biased measurements. Drifting chambers are also complicated for several reasons, e.g., the presence of obstacles in the streams or in terms of logistics, as the chambers may travel far during measurement periods.

While establishing efficient methods for running water gas emissions are needed to improve the global GHG budgets, progress in chamber based methods is prevented by the lack of comparative assessments of anchored versus drifting chambers. In this study, we compared measurements of GHG fluxes and the gas exchange velocity using drifting and anchored chambers in various streams and rivers. Because chamber performance is expected to depend strongly on chamber design, the field experiments were conducted using three different chamber types. In laboratory experiments, we analyzed the flow field and the turbulence under both anchored and drifting chambers at different flow velocities. The primary objective of this study was to answer the question: Do anchored chambers produce reliable measurements of localized GHG fluxes in running waters?

2 Methods

2.1 Chamber measurements in the field

Field measurements were conducted in nine different rivers and streams in Germany and Poland using three different chambers (Table 1). All three data sets included *anchored measurements*, where the chambers were tethered to stay at a fixed position as well as *drifting*

measurements, where the chambers were freely moving with the current. In two of the data sets (A and B), the temporal change of CO_2 and CH_4 concentration in the chamber headspace was measured on a boat using infrared gas analyzers (A: OA-ICOS gas analyzer, UGGA, Los Gatos Research Inc. USA, B: FTIR analyzer, Gasmet 4010, Gasmet, Finland). In the third data set (C), the gas concentration was measured using a built-in and low-cost CO_2 sensor (ELG, SenseAir, Sweden). The chamber used in (C) is described in detail elsewhere (Bastviken et al., 2015).

The chamber flux measurements were supplemented by measurements of dissolved gas concentrations (CO_2 and in data set A and B also CH_4) in the stream water and in the atmosphere (Table 1). Additional measurements include water temperature and near-surface current velocity, which was measured at selected sites within the study reaches using acoustic or electromagnetic current meters. More details on sampling and instrumentation are provided in Appendix A.

The flux F (mmol m^{-2} d^{-1}) of CO_2 (all data sets) and CH_4 (parts of data set A and B), was calculated from the observed rate of change of the mole fraction S (ppm s^{-1}) of the respective gas in the chamber using (Campeau and Del Giorgio, 2014):

$$F = (S \cdot V / A) \cdot t_1 \cdot t_2 \quad (1)$$

Where V is the chamber gas volume (m^3), A is the chamber area (m^2), t_1=8.64 × 10^4 s d^{-1} is the conversion factor from seconds to days, and t_2 is a conversion factor from mole fraction (ppm) to concentration (mmol m^{-3}) at *in-situ* temperature (T in K) and atmospheric pressure (p in Pa), according to the ideal gas law:

$$t_2 = p / (8.31 \text{ J K}^{-1} \text{ mole}^{-1} \cdot T) \cdot 1000 \quad (2)$$

The gas exchange velocity of the respective gas at in-situ temperature k (m d^{-1}) was estimated from measured fluxes as:

$$k = F / (K_H \cdot (p^{water} - p^{air})) \quad (3)$$

using the partial pressure of CO_2 and CH_4 in the stream water (p^{water}) and in the atmosphere (p^{air}). The partial pressures were obtained by multiplication of the measured mole fraction with atmospheric pressure. K_H is the temperature-dependent Henry constant (mmol m^{-3} Pa^{-1}) (Goldenfum, 2011). The *in-situ* gas exchange velocities were converted to a standardized (independent of temperature and gas diffusivity) exchange velocity k_{600} using the Schmidt number dependence:

$$k_{600} = k \cdot (600 / Sc)^{-n} \quad (4)$$

where the temperature-dependent Schmidt numbers (*Sc*) of both gases were estimated according to Goldenfum (2011). The Schmidt-number exponent *n* describes the dependence of the gas exchange velocity of a particular gas on the diffusion coefficient of this gas in water. We used n=0.5, which showed best agreement with measurements for wave-covered and turbulent water surfaces (Jähne and Haußecker, 1998).

2.2 Turbulence measurements in the lab

The flow fields under freely drifting and anchored chambers were measured using particle image velocimetry (PIV) in a 3 m long laboratory flume. The chamber type and geometry was identical to the chamber in data set C (Table 1). The flow field under the drifting chamber was measured for 50 repeated chamber runs (58 s cumulative velocity observations under the chamber) at a mean flow velocity of 0.10 m s^{-1}, the highest flow velocity that could be realized in the flume. Measurements under anchored chambers were performed for 90 s at a mean flow velocity of 0.10 m s^{-1}. Additional measurements were performed at reduced mean flow velocities of 0.08 and 0.06 m s^{-1}. As a reference, the undisturbed flow field without chambers was measured for 90 s. Due to the limited length of the laboratory flume it was not possible to measure gas fluxes or estimate the gas exchange velocities.

The flow fields were analyzed by illuminating neutrally buoyant seeding particles (diameter of 20 µm, polyethylene) within a thin light sheet produced by a double-pulse laser

142 (DualPower 200-15, DantecDynamics) with 5 ms between pulses. The sampling frequency
143 was 7.5 Hz. Images were recorded in a 145 × 145 mm² field of view with a charge-coupled
144 device (CCD) camera (FlowSense 4M MKII, 2048 × 2048 pixels, DantecDynamics). The
145 camera was inclined by 30° to the horizontal, which allowed for observing flow velocities
146 below the chamber.
147 The two-dimensional (longitudinal and vertical) flow velocities within the field of view were
148 estimated using an adaptive correlation algorithm (Dynamic Studio, DantecDynamics) with a
149 final spatial resolution of 2.6 × 2.6 mm². The longitudinal extent of the observed flow fields
150 (433 mm for anchored and 395 mm for drifting chambers) covered the complete chamber
151 diameter and velocities are reported as a function of distance from the leading chamber edge
152 in both the anchored and the drifting deployment.
153 The turbulent kinetic energy (*TKE*) was estimated by assuming isotropy in the unresolved
154 velocity component as:

155 $$TKE = \frac{3}{4}\overline{(u'^2 + w'^2)} \quad (5)$$

156 where u' and w' denote the temporal fluctuations of the longitudinal and vertical velocity
157 component, respectively, and the overbar denotes temporal averaging.

158 ## 2.3 Statistics

159 The mean fluxes measured with anchored and drifting chambers in the respective field data
160 sets were compared using paired *t*-tests, comparisons between the data sets were performed
161 using 2-sample *t*-tests. Spearman rank correlations coefficients (r_S) were estimated when
162 testing for correlations between gas exchange velocities from anchored and drifting chambers
163 for each data set. All analyses were performed at a significance level $p<0.05$, unless stated
164 otherwise.

3 Results

3.1 Drifting vs. anchored chamber measurements in the field

In all measurements, the CO_2 and CH_4 fluxes were positive, i.e. the streams were sources of both gases to the atmosphere. While the mean CO_2 fluxes measured by drifting chambers did not differ significantly among the data sets B and C, they were about seven-fold higher in data set A (Table 2). In all data sets, anchored chamber fluxes were significantly higher than the corresponding drifting chamber fluxes.

Gas exchange velocities k_{600} estimated from CO_2 measurements in the drifting chamber deployments ($k_{600\_CO2\_d}$) ranged between 0.2 and 8.1 m d^{-1}. They varied widely within each data set (Table 2), but in contrast to the current velocities mean values of $k_{600\_CO2\_d}$ did not significantly differ among the data sets. In all data sets, however, k_{600} from anchored chambers ($k_{600\_CO2\_a}$) differed significantly from that of drifting chambers (Fig. 1A). Except for data set A, both were weakly correlated to each other (r_S = 0.49, p=0.01 and r_S = 0.76, p<0.001 for data set B and C, respectively) (Fig. 1B). With only a few exceptions, the gas exchange velocities under anchored chambers were higher than those under drifting chambers with individual measurements, $k_{600\_CO2\_a}$ being up to 20 times higher than $k_{600\_CO2\_d}$. The average ratio of both velocities was 2.2, 6.2 and 4.0 for data set A, B and C, respectively (Table 2).

When both gases were measured, the gas exchange velocities estimated from CO_2 fluxes were strongly correlated to those estimated from CH_4 measurements for both deployment types. Small but significant differences were observed between $k_{600\_CO2\_d}$ and $k_{600\_CH4\_d}$, whereas the CO_2 based estimates were on average slightly higher in data set A and lower in data set B (Fig. 1A). In accordance with the CO_2 based estimates, k_{600} estimated from CH_4 was higher under anchored than under drifting chambers (Table 2) and the ratio k_{600_a} / k_{600_d} did not differ significantly between both gases.

When combining all data sets, there was no correlation between gas exchange velocities and the measured current velocity for drifting chambers for either CO_2 or CH_4 (Fig. 2A). However, for anchored chamber deployments, k_{600_a} was positively correlated to current speed in data set A (r_S=0.54, p=0.02) and B (r_S=0.7, p<0.001). The ratio of the gas exchange velocities estimated from both deployment types was positively correlated to current speed when all three data sets were combined (r_S=0.66, p<0.001), but no significant correlations were observed within the individual data sets (Fig. 2B).

3.2 Flow field and turbulence under chambers

The laboratory measurements revealed pronounced differences in the flow fields and turbulence under the anchored and drifting chambers. The mean longitudinal flow velocity was strongly reduced within the submerged part of the anchored chamber and increased below the submerged chamber edge. Recirculating eddies were formed under the leading (upstream) edge of the chamber (vector graphs of the mean velocity distributions are provided in Appendix B). These eddies detached and injected turbulence below the chamber (Fig. 3). The turbulent kinetic energy which was produced by the submerged edge of the anchored chambers increased with increasing current speed (Appendix B). Under the drifting chambers, the flow velocities were slightly enhanced below the submerged chamber edge, but no recirculating eddies were formed.

The penetration depth of the chamber edges varied with time as the chamber moved vertically on the rough water surface (see Appendix B for snapshots of instantaneous velocity distributions and chamber penetration). However, at the same flow velocity the average penetration depth of the anchored chamber was higher than that of the drifting chamber (Fig. 3).

4 Discussion

4.1 Chamber bias in anchored deployments

Our field observations showed consistently higher gas exchange velocities and gas fluxes measured with anchored in comparison to freely drifting chambers in a variety of small streams with flow velocities between 0.08 and 0.8 m s^{-1}. Detailed observations of the flow field and turbulence under both types of chambers in the laboratory revealed a reduction of mean flow velocity and the generation of chamber-induced turbulence due to the shedding of eddies at the upstream part of the submerged edge of the anchored chamber. Under identical hydraulic conditions, anchored chambers penetrated deeper into the water, which we attribute to a partial diversion of the strong horizontal drag force imposed by the flow into the vertical direction. In combination, horizontal current shear and deeper penetration caused an increase in magnitude of chamber-induced turbulence with increasing difference in velocity between the water flow and the chamber (Fig. B1). This mechanism has been suggested in previous studies of floating chamber performance in water bodies, although there are mixed results regarding its importance (Cole et al., 2010;Gålfalk et al., 2013;Vachon et al., 2010).

The laboratory observation agrees with our field measurements, where the ratio of the fluxes measured with anchored and with drifting chambers was comparably small at flow velocities <0.2 m s^{-1}. However, even at low flow velocities, the gas exchange velocity was enhanced by more than a factor of two in the anchored deployment. At higher flow velocities (> 0.2 m s^{-1}) typical for rivers and streams, chamber-induced turbulence obviously dominated the gas flux into the anchored chambers.

The large (several-fold) potential overestimation of fluxes measured with anchored chambers calls into question its suitability for application in running waters, particularly at high flow rates. This agrees with the observations of Teodoru et al. (2015) who reported a linear

238 dependency of the gas exchange velocity under anchored chambers on the water velocity
239 relative to the chamber in a large river.

240 ## 4.2 Correction methods and chamber optimization

241 The correlation of the anchored chamber gas exchange velocity with flow velocity observed
242 in our study could provide a potential means for correcting the artificial chamber flux, if the
243 corresponding drifting chamber gas exchange velocity was also a function of flow velocity.
244 However, no such correlation was present in our field observations, indicating that near-
245 surface flow velocity is a poor predictor for the gas exchange velocities in streams. Therefore,
246 it can be expected that river depth and bed roughness affect the near-surface turbulence more
247 than flow velocity (Moog and Jirka, 1999;Raymond et al., 2012).
248 As the correction of the effects of chamber-induced turbulence on measured fluxes seems
249 unlikely, it would be more reasonable to optimize the chamber design to completely avoid or
250 to at least reduce this effect. The rectangular chamber B produced the largest error, although it
251 remained unclear from our measurements whether this was caused by the geometry of the
252 chamber or by the high flow velocity in data set B. On this basis, we recommend the use of
253 more streamlined circular chambers to minimize the error under drifting conditions. Crawford
254 et al. (2013) and McMahon and Dennehy (1999) used streamlined (canoe-shaped) instead of
255 cylindrical or rectangular chambers to minimize the generation of chamber-induced
256 turbulence at the upstream chamber edge during anchored chamber deployments. However,
257 they did not provide evidence that this goal was reached.
258 Another approach to minimize the bias of anchored chambers would be to design chambers
259 without submerged rigid walls. Submergence of the chamber edges can be avoided
260 completely by using a thin plastic foil which adheres to the water surface to seal the chamber
261 headspace (Fig. 4A). Laboratory (PIV) measurements of the flow field were performed under
262 a foil, mimicking a chamber deployed in anchored mode. The measurements revealed a strong

reduction of flow disturbances and chamber-induced turbulence (Fig. 4) in comparison to both anchored and drifting chambers. Such "flying chambers" require a frame to keep the chamber above the water surface, which can be supported by floats at a larger lateral distance to the chamber or, in small streams, also by a fixation at the river bank.

4.3 Implications for chamber-based flux measurements

Our study clearly shows that anchored chambers strongly overestimate the gas flux in running water and are not suited to quantify greenhouse gas fluxes in streams and rivers. One possible way forward to reduce this bias while still maintaining the practical advantages of the anchored chambers could be flying (anchored) chambers with flexible foil sealing at the water surface. Drifting chambers provide a practical and reliable solution, although they are not free of potential spatial bias. Because their measurement locations are difficult to control, their trajectories may not be representative for the areal mean flux from the study reach. Regions with locally enhanced turbulence, e.g., stream-reaches with large emerging roughness of the river bed, cannot be surveyed with drifting chambers, however the gas exchange velocity is highest at these sites (Moog and Jirka, 1999). Similarly, mean-flow trajectories may bypass backwaters and regions of reduced flow velocity along the stream banks. Observations in reservoirs and river impoundments revealed that the enhanced sedimentation of particulate organic matter can make these zones emission hot spots (Maeck et al., 2013;DelSontro et al., 2011). Anchored chamber deployments may provide a useful extension of drifting chamber measurements at such sites, if the flow velocity is sufficiently small. To truly validate a reliable chamber method for small streams, a multi-method comparison study, including tracer additions, should be performed.

This study shows that flux chamber approaches to measure GHG fluxes from running waters have a high potential, given sufficient knowledge about appropriate chamber design and

deployment approaches. Thus, flux chambers are emerging as an important method to constrain greenhouse gas fluxes from stream networks.

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Appendices

Appendix A: Additional information on the field data sets

A1: Data set A

Field measurements of five streams in North Central European Plains in Germany and Poland were conducted during October 2014. Gaseous CO_2 and CH_4 emissions were measured at the water-air interface with a drifting chamber attached to an Ultraportable Greenhouse Gas Analyzer (UGGA; Los Gatos Research, Inc., USA). The chamber was connected to the UGGA placed in a boat via two gas tight tubes (Tygon 2375), creating a circulation of air being sucked in and pumped out. For the anchored measurements, we tethered the chamber to a rack in the middle of the respective stream, in which we placed the sensors for continuously dissolved CO_2 and CH_4 measurements (HydroC™; CONTROS Systems & Solutions GmbH, Germany). Subsequently, we floated down a predefined stream section with the same chamber following freely the boat or vice versa at the speed of the current. During the chamber measurements, the UGGA continuously measured the gaseous CO_2 and CH_4 accumulation in the chamber (frequency 1 s). Flow velocity was measured with an Acoustic Digital Current Meter (OTT, Germany).

A2: Data set B

Measurements were performed on the Bode River between Egeln-Nord and Staßfurt on 7 April 2014 (summer base flow 7.7 $m^3 s^{-1}$) and 12 March 2015 (winter high flow 12.8 $m^3 s^{-1}$). The flux of CO_2 and CH_4 between water and atmosphere was measured by a rectangular floating chamber, which was connected to an FTIR analyzer (GASMET 4010, Finland). Measurements were performed from a boat while drifting down the river. For a single measurement, the chamber was placed at the water surface for up to five minutes and CO_2 and

CH_4 change inside the chamber was measured every 30 s. To compare drifting and fixed chamber measurements, the boat was then stopped by an anchor and measurements continued for another 3-5 min. During this stationary measurement, current velocity was measured with an electromagnetic current meter (MF-Pro, Ott, Germany) and water temperature were measured by hand held probes (ProfiLine Multi,WTW, Germany).

The concentration of CO_2 in the water was continuously measured by a submersible probe (HydroC™; CONTROS Systems & Solutions GmbH, Germany). Additionally samples for CH_4 analysis were taken in plastic syringes and later analyzed by headspace GC.

Water temperature was continuously measured by temperature loggers (Tidbit, Onset, U.S.A.). The barometric pressure was recorded by the FTIR analyzer.

Under drifting conditions the CH_4 flux was often below the detection limit while there was always a positive CH_4 flux in anchored chamber deployments.

A3: Data set C

Chambers with a cross-sectional area of 0.066 m^2 and volume of 6.8 L were covered by aluminum foil to reduce the internal heating and equipped with a Styrofoam material to keep the chamber body floating on water surface. The chambers were equipped with an internal CO_2 logger system that is positioned inside the headspace of the chamber (Bastviken et al., 2015). The non-dispersive infrared (NDIR) CO_2 logger (ELG, SenseAir, Sweden, www.senseair.se) measures CO_2 in the range of 0-5000 ppm. The logger measures simultaneously CO_2, temperature and relative humidity, and operates at temperature and humidity of 0-50 ºC and 0-99% (non-condensing conditions) respectively. The loggers were calibrated by the manufacturer and operated with 9 VDC batteries. The measurement interval was adjusted to be 30 s, more information of technical specifications are provided elsewhere (Bastviken et al., 2015).

Chambers were deployed fixed at a certain position (anchored) and freely drifting. Triplicate measurements were conducted during each drifting run, and three runs were conducted at each site. The anchored chambers were then used for measuring the flux of CO_2 at different locations along the pathways of the drifting chambers. The chamber flux measurements were supplemented by measurements of dissolved gas CO_2 and CH_4 concentrations in the stream waters at each anchored stations for each run. Continuous measurements of CO_2 and methane in the middle of the stream were conducted using a membrane equilibrator (Liqui-Cel MiniModule, Membrana, USA) connected with an Ultraportable Greenhouse Gas Analyzer (UGGA; Los Gatos Research, Inc., USA). The water samples were pumped through the membrane contactor using a peristaltic pump at a constant flow rate.

Appendix B: Mean flow and turbulence under anchored chambers at different current speeds

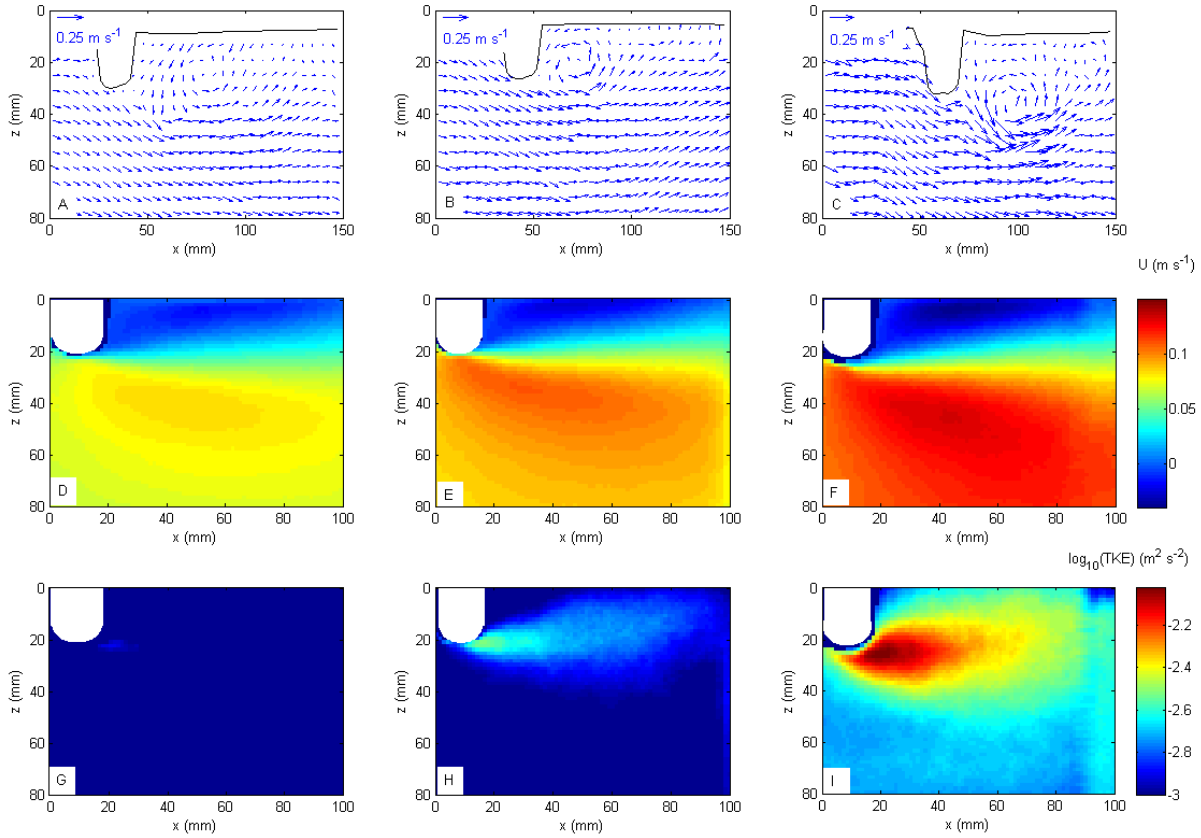


Fig. B1: Laboratory measurements of flow velocity and turbulence under anchored chambers at different mean current speeds (left: 0.06m s^{-1}, middle: 0.08 m s^{-1}, right: 0.10 m s^{-1}. A-C) shows examples of instantaneous velocities around the leading edge of the chambers. The water surface and the leading chamber edge are marked by solid black lines. D-F) temporal mean longitudinal flow velocity (*U*). G-I) mean turbulent kinetic energy (TKE). The chamber edges are masked out (white) and regions without sufficient observations (< 90 s for the anchored cases) are displayed in dark blue. The direction of flow was from left to right, *x* and *z* refer to longitudinal distance and depth, respectively.

Tables

Table 1

Table 1: Summary of the three data sets obtained in field measurements. Pictures show the three different chambers used for the anchored and drifting approach. Additional information about the sampling procedures are provided in the Supplementary Information.

Data set	**A**	**B**	**C**
			
Site	5 different streams North-Central European Plains in Germany and Poland	Bode river, Harz mountains, Central Germany	3 different streams, Upper Rhine Valley, South-West Germany
Chamber volume (m^3)	0.0168	0.0147	0.0068
Chamber area (m^2) (shape)	0.126 (circular)	0.098 (rectangular)	0.066 (circular)
Chamber height (m)	0.175	0.15	0.13
Penetration depth (m)	0.018	0.023	0.025
Chamber gas measurement	LosGatos, CO_2, CH_4 on boat	FTIR analyzer (GASMET, Finland) on boat	Built-in low-cost CO_2 logger (ELG by SenseAir, Sweden)
Dissolved gas measurement	Contros CO_2 and CH_4	Contros CO_2, CH_4 with GC	UGGA with membrane contactor
Drifting measurements	following boat or vice versa	Freely drifting while followed with boat	Freely drifting
Anchored measurements	Tethered to a rack in the middle of the stream	Tethered to anchored boat	Tethered with rope from above
Number of measurements	At 5 sites: 2-5 pairs of anchored chamber measurements (upstream) and subsequent floating chamber runs	For two different discharge situations: 10-13 pairs of subsequent drifting and anchored chamber measurements down the river using a single chamber	At 3 sites: 2-3 subsequent floating chamber runs and 5 parallel anchored chambers distributed along the trajectory of the floating chamber

384 Table 2

385 **Table 2:** Discharge rate, flow velocities, gas fluxes (F_{CO2}, F_{CH4}), and gas exchange velocities
386 (k_{600_CO2}, k_{600_CH4}) estimated from drifting (subscript d) and from anchored (subscript a)
387 chambers during the three field campaigns (A-C, cf. Table 1). Except for discharge, all values
388 are given as mean ± standard deviation.

Data set No. of samples *n*	**A** n_{CO2}=18 n_{CH4}=18	**B** n_{CO2}=27 n_{CH4}=9	**C** n_{CO2}=24 n_{CH4}=0
Discharge (m^3 s^{-1})	0.6 – 1.4	7.7 – 12.8	0.1 – 7.6
Flow velocity (m s^{-1})	0.21 ± 0.07	0.60 ± 0.12	0.30 ± 0.07
F_{CO2_a} (mmol m^{-2} day^{-1})	742 ± 282	302 ± 148	103 ± 47
F_{CO2_d} (mmol m^{-2} day^{-1})	363 ± 139	55 ± 30	49 ± 36
$k_{600\_CO2\_a}$ (m day^{-1})	6.5 ± 1.4	17 ± 6.4	4.1 ± 2.8
$k_{600\_CO2\_d}$ (m day^{-1})	3.3 ± 1.1	3.2 ± 1.5	2.1 ± 2.5
$k_{600\_CO2\_a}$ / $k_{600\_CO2\_d}$	2.2 ± 0.9	6.2 ± 3.2	4.0 ± 5.0
F_{CH4_a} (mmol m^{-2} day^{-1})	4.31 ± 1.35	1.55 ± 0.71	-
F_{CH4_d} (mmol m^{-2} day^{-1})	2.12 ± 0.86	0.37 ± 0.16	-
$k_{600\_CH4\_a}$ (m day^{-1})	6.0 ± 1.4	23.0 ± 10.8	-
$k_{600\_CH4\_d}$ (m day^{-1})	2.9 ± 0.9	5.5 ± 2.4	-
$k_{600\_CH4\_a}$ / $k_{600\_CH4\_d}$	2.3 ± 1.0	4.8 ± 2.1	-

389

Figures

Figure 1

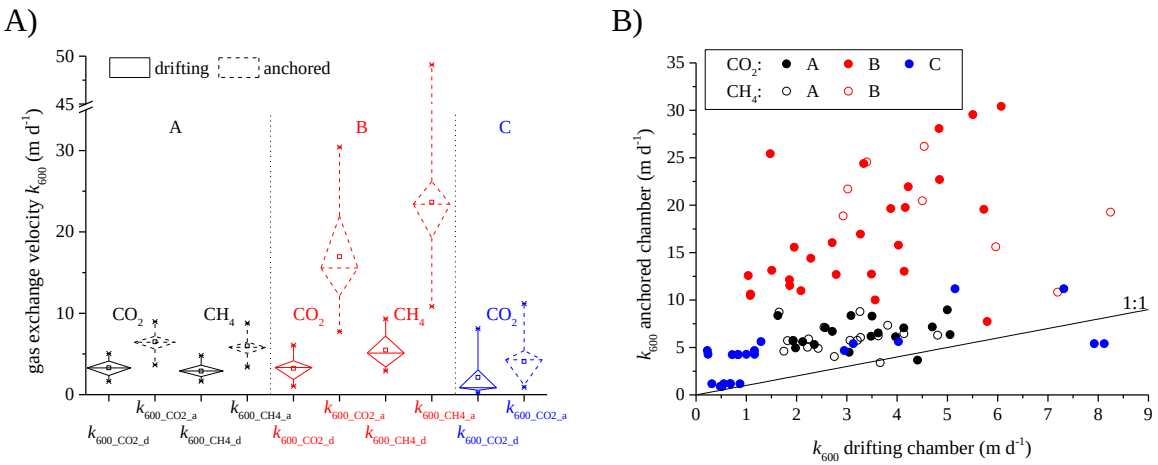


Fig. 1: A) Box plots of the standardized gas exchange (k_{600}) velocity measured using drifting (solid lines) and anchored (dashed lines) flux chambers in data set A (black), B (red) and C (blue). The diamond-shaped boxes encompass the 25-75 percentile range, whiskers show minimum and maximum, open squares and horizontal lines mark mean and median values, respectively. B) k_{600} estimated from anchored chamber deployments versus that from drifting chambers for the data sets A-C (color). Filled symbols show k_{600} estimated from CO_2 fluxes, open symbols are based on CH_4 fluxes. The solid line shows a 1:1 relationship.

Figure 2

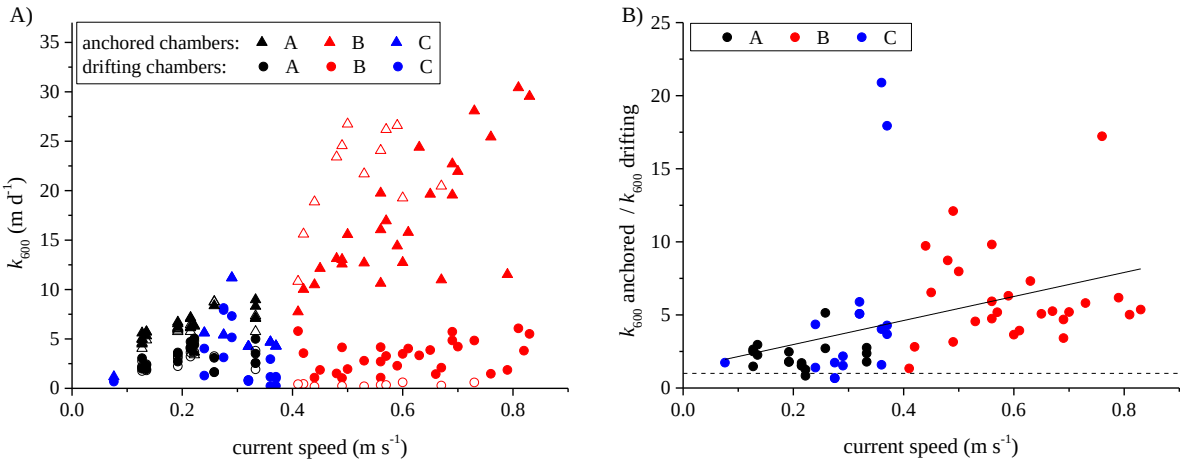
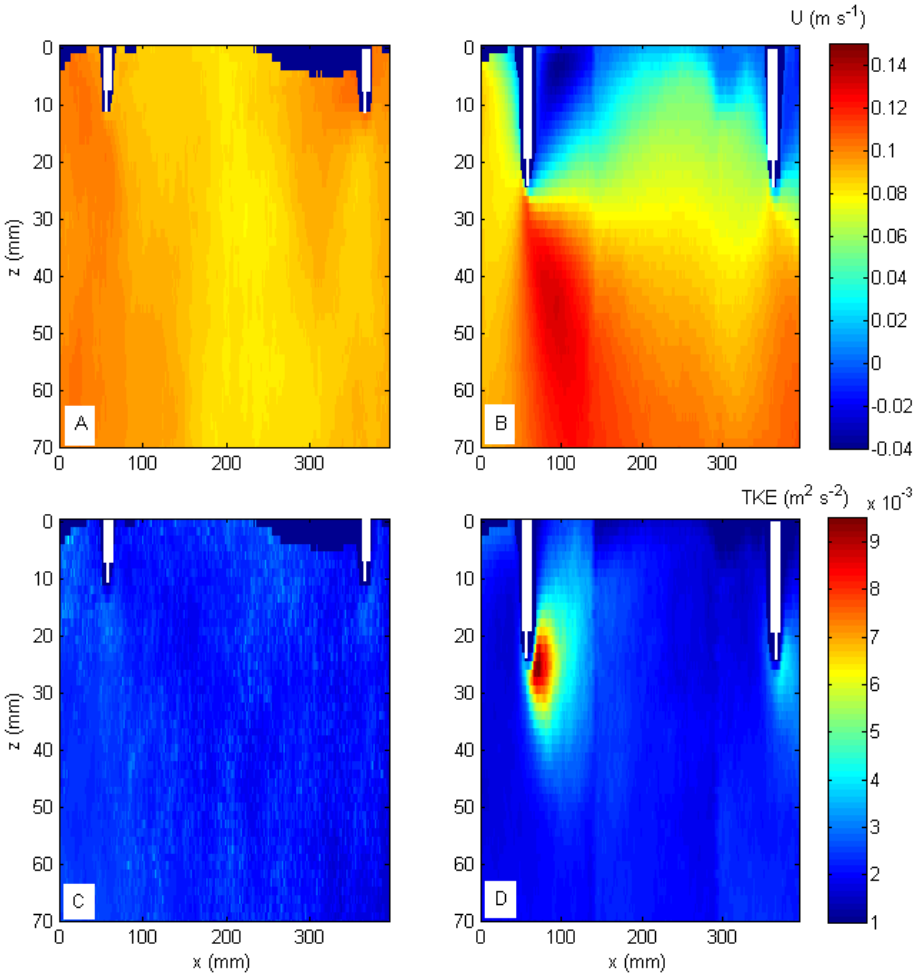


Fig. 2: A) Gas exchange velocity k_{600} from anchored (triangles) and drifting (circles) chambers versus current velocity for the three field data sets (A-C, colors). Filled symbols show data obtained from CO_2, open symbols are based on CH_4 fluxes. B) Ratio of the gas exchange velocities from anchored and drifting chambers versus current speed (filled symbols: CO_2, open symbols: CH_4, symbol color indicates data set). The dashed line indicates a constant ratio of one and the solid line shows a linear regression of the combined data sets (r_S=0.66, p<0.001).

402 Figure 3



403

404 **Fig. 3:** Laboratory measurements of the mean longitudinal flow velocities (*U*) A) below a
405 drifting and B) below an anchored chamber. Mean turbulent kinetic energy (TKE) of the flow
406 fields below C) the drifting chamber and D) the anchored chamber. *z* and *x* refer to depth and
407 longitudinal distance respectively. Chamber edges are masked out (white) and regions without
408 sufficient observations for temporal averaging are marked by dark blue color. The flow
409 direction is from left to right and the mean flow velocity was 0.1 m s^{-1}.

410

411 Figure 4

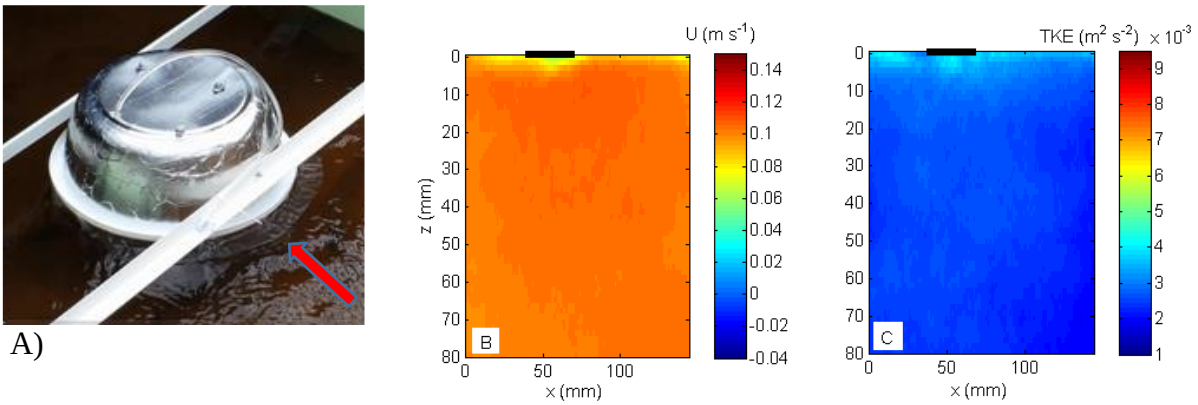


Fig. 4: A) Flying chamber design without penetration of the water surface by the chamber edges but using a plastic foil collar (marked by the red arrow) for sealing. The chamber is fixed above the water surface by a supporting frame. B) Distribution of mean longitudinal flow velocities (*U*) and B) turbulent kinetic energy (*TKE*) of the flow field below the front edge of a static foil (marked by black bar) at the water surface. The direction of flow was from left to right, *x* and *y* refer to longitudinal distance and depth, respectively. The mean flow velocity was 0.10 m s^{-1}. Color scales are identical to that of Fig. 3.

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