# A chemical kinetics theory for interpreting the non-monotonic temperature dependence of enzymatic reactions

Jinyun Tang<sup>1</sup>, William J. Riley<sup>1</sup>

<sup>1</sup>Department of Climate Sciences, Earth and Environmental Sciences Area, Lawrence Berkeley National Laboratory, Berkeley, 5 CA, USA.

Correspondence to: Jinyun Tang (jinyuntang@lbl.gov)

Abstract. One notable observation of enzymatic chemical reaction is that, for a given abundance of enzymes and substrates, temperature increases cause reaction rates to first increase consistent with the Arrhenius relationship, then plateau, and finally fall off quickly to zero at high temperatures. While many mathematical functions have been used to describe this pattern, we

- 10 here propose a chemical kinetics theory which successfully replicates this observation and provides insights into the processes responsible for these dynamics. The chemical kinetics theory combines the law of mass action, von Smoluchowski's diffusionlimited chemical reaction theory, and Eyring's transition state theory. This new theory reveals that the thermally reversible enzyme denaturation ensured by the ceaseless thermal motion of molecules and ions in an enzyme solution explains the plateau and subsequent decrease of chemical reaction rates with increasing temperature. The temperature-dependent affinity parameter
- 15 (*K*) that relates enzymes and substrates through their binding also affects the shape of the emergent temperature response. We demonstrate that with an increase in substrate availability, *K* shifts the optimal temperature, where reaction rates plateau, towards higher values. Further, we show that the chemical kinetics theory accurately represents 12 sets of published enzyme assay data, and includes the popular mechanistic model by Ratkowsky et al. (2005) as a special case. Given its good performance and solid theoretical underpinning, we believe this new theory will facilitate the construction of more
- 20 mechanistically-based environmental biogeochemical models.

### **1** Introduction

When an enzyme-catalysed chemical reaction is monitored under a range of temperatures, one often observes that the reaction rate first increases with temperature in a manner following the Arrhenius function, peaks at some temperature, and then falls off quickly to zero when the temperature is too high for the enzyme to function (Sharpe and DeMichele, 1977;

25 Peterson et al., 2004). As enzymes catalyse almost every chemical reaction relevant to life, this temperature response has also been observed for growth and respiration rates that emerge from the interactions among myriads of chemical reactions in an organism (Precht et al., 1973). In order to describe this non-monotonic relationship between enzymatic reaction rates and temperature, many empirical and mechanistically-based functions have been proposed. Sharpe and DeMichele (1977) proposed a model that

- 30 incorporates the empirical observation of thermally reversible enzyme denaturation (e.g., Sizer, 1943; Alexandrov, 1964) and the transition state theory (Eyring, 1935). They assumed that enzymes undergo reversible transitions between three states: a cold-induced inactive state, a heat-induced inactive state, and an active state capable of catalysis. By assuming reactions to be substrate unlimited, they obtained a model with five thermodynamic parameters that is able to almost perfectly fit published temperature-dependent growth rates of eight poikilothermic organisms (see their Figures 5 and 6). We note that the
- 35 applicability of the Sharpe-DeMichele model to growth rates of an organism is based on the assumed existence of control by master enzymes (Johnson and Lewin, 1946). Motivated by the success of Sharpe and DeMichele (1977) and the work on thermally reversible protein denaturation by Murphy et al. (1990), Ratkowsky et al. (2005) grouped the two inactive states into one, and, again assuming no substrate limitation, derived a model with two thermodynamic parameters and two enzyme informatic parameters, which was able to very accurately fit 35 sets of observed temperature-dependent bacterial growth rates.
- 40 The model by Ratkowsky et al. (2005) was later used by Corkrey et al. (2012) and Corkrey et al. (2014) to successfully interpret the temperature-dependent growth rates of many more poikilothermic organisms. Ghosh et al. (2016) extended the Ratkowsky et al. (2005) model by including the thermally reversible denaturation of many enzymes and proteins informed by proteomics, and were able to satisfactorily interpret the measured temperature-dependent growth rates of mesophiles and thermophiles.

Recently, Hobbs et al. (2013) argue that enzyme denaturation is not necessary to interpret the non-monotonic dependence of enzymatic reaction rates on temperature. Instead, they proposed the macromolecular rate theory (MMRT), which assumes that the change in heat capacity associated with enzyme catalysis and its consequent effect on the temperature dependence of the Gibbs free energy of activation can describe the temperature dependence of enzyme activity. Following the success of Hobbs et al. (2013) on modeling the temperature dependence of single-enzyme catalyzed reactions, Schipper et al. (2014) showed that MMRT better fits measured relationships between soil biogeochemical rates and temperature, including those for aerobic respiration, methane oxidation, nitrification, and denitrification, than Arrhenius-like or Q<sub>10</sub> functions. Later, Alster et al. (2016) demonstrated that MMRT was successful at capturing the temperature dependence of extracellular enzyme activities, including those of β-glucosidase, leucine aminopeptidase, and phosphatase. Following these studies, Liang et al.

(2018) recommended that MMRT should be used for improved description of the measured relationship between plant leaf respiration and temperature. Recently, Alster et al. (2020) advocated that MMRT should be used widely to represent the

55 temperature dependence of many types of soil biogeochemical processes.

Besides the mechanistically-based models mentioned above, there are quite a number of empirically-based models described in the literature, e.g., the log-polynomial function (O'Sullivan et al., 2017), the four-parameter square root function (Ratkowsky et al., 1983), the Zwietering model (Zwietering et al., 1991), the Cardinal temperature model with inflection (Lobry et al., 1991), and others. More examples can be found in Grimaud et al. (2017) and Noll et al. (2020).

- 60 While the mechanistically-based and empirically-based models described above have been quite successful in fitting the relationship between measured rates and temperature, they do not account for the fact that the overall temperature response may be affected by substrate availability. This issue is acknowledged, for example, when Sharpe and DeMichele (1977) put forward their model and may be a barrier for developing biogeochemical models that strive to resolve the temperature dependence of biogeochemical rates mechanistically.
- In the following, we develop the chemical kinetics model to deliver a comprehensive description of the nonmonotonic relationship between temperature and enzymatic reaction rates. The model incorporates the observation that thermally-reversible enzyme denaturation always occurs due to the thermal motion of molecules and ions in the solution of enzyme proteins (Finkelstein and Ptitsyn, 2016), and three well-established theories of chemical reactions: (1) law of mass action (Koudriavtsev, 2011), (2) von Smoluchowski's diffusion-limited chemical reaction theory (von Smoluchowski, 1917),
- 70 and (3) Eyring's transition state theory (Eyring, 1935). We evaluated the theory with 12 datasets of enzyme essays and then discuss how this new theory provides mechanistic explanations and accurate representations of the temperature dependence of biogeochemical reaction rates. We leave out the temperature-dependent irreversible enzyme denaturation, but note that it needs to be included in a dynamic model (Tang and Riley, 2015;Alvarez et al., 2018).

## 2. Methods

75 2.1 The enzymatic reaction problem

We consider the simplest form of enzymatic reactions:

$$E_n + S \stackrel{k_1^+}{\rightleftharpoons} E_n S \stackrel{\nu_{max}}{\longrightarrow} E_n + P, \tag{1}$$

where  $E_n$  is the concentration of free enzymes whose conformation structure is in the active state and able to carry out the catalysis, *P* is product concentration, *S* is substrate concentration,  $E_nS$  is enzyme-substrate complex concentration, and  $k_1^+$ ,  $k_1^-$ , and  $v_{max}$  are temperature (*T*) dependent kinetics parameters. Although it is not necessary for the validity of Michaelis-Menten kinetics (Briggs and Haldane, 1925), for scaling purposes,  $v_{max}$  (the maximum enzymatic catalysis rate) is often assumed to be much greater than  $k_1^-$  (Tang and Riley, 2017; Kooijman, 2009; Holling, 1959; Aksnes and Egge, 1991; Van Slyke and Cullen, 1914). Throughout this study, we take all variables to be in ISO units, and provide a list of all variables and their explanations in the Appendix.

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Figure 1: In the chemical kinetics theory, the Gibbs free energy of activation  $\Delta G_V$  is a linear function of temperature, i.e.  $\Delta G_V = \Delta H_V - T\Delta S_V$ , with the enthalpy of activation  $\Delta H_V$  and the entropy of activation  $\Delta S_V$  both being constant. This behavior of  $\Delta G_V$ , along with the thermally reversible denaturation of the enzymes (as depicted by the inactive and active states here), leads to the non-monotonic temperature response of catalysis rate. Other variables are defined in the main text.

By applying the law of mass action and the quasi-steady-state-approximation (Borghans et al., 1996) to equation (1),

90 i.e.  $k_1^+ E_n S = (v_{max} + k_1^-)C$ , with *C* being the concentration of enzyme-substrate complex  $E_n S$ , we obtain Michaelis-Menten equation for the overall reaction rate *F*:

$$F = v_{max}C = v_{max}\frac{E_{nt}S}{K+S},\tag{2}$$

where  $K = v_{max}/k_1^+$  is the half saturation parameter (by taking the usual assumption  $v_{max} \gg k_1^-$  (Tang and Riley, 2017)), and  $E_{nt}$  is the total concentration of enzymes that are able to form enzyme-substrate complexes, i.e.  $E_{nt} = E_n + C$ .

We next describe how the chemical kinetics theory represents the temperature dependence of F.

#### 95 2.2 The chemical kinetics theory

In studying proteins in an aqueous solution, it was observed that proteins may spontaneously unfold into inactive states, which for enzymes means losing their catalysis capability (Nojima et al., 1977; Finkelstein and Ptitsyn, 2016). By taking advantage of the thermal motion, the unfolded inactive enzyme proteins can also refold into their active state, regaining their catalysis capability (Oliveberg et al., 1995). Therefore, as thermal motion is ceaseless for all temperatures that are physiologically amenable to enzymatic reactions, it is safe to assert that at any time, even without irreversible denaturation, some enzymes are in inactive states not capable of catalysing their specialized chemical reactions.

Chemical kinetics theory (Figure 1) incorporates the observation of thermally reversible denaturation by considering that a fraction  $(1 - f_E(T))$  of the enzymes  $(E_t)$  are in the thermally reversible denatured inactive state (e.g., Finkelstein and Ptitsyn, 2016; Ghosh and Dill, 2009), so that the catalytically active enzyme concentration  $E_{nt}$  is  $f_E(T)E_t$ . Further, by

105 thermodynamics, Jin and Bethke (2003) showed that, in addition to enzyme catalysis, the chemical reaction is driven by a thermodynamic potential parameterized through a function  $f_R(T)$ , which is a function of  $\Delta G_R$ , the Gibbs free energy of the chemical reaction of converting the reactants into products. These turn equation (2) into

$$F = \frac{v_{max} f_E(T) E_t S}{K+S} f_R(T), \tag{3}$$

where

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$$v_{max} = v_{max,0} f_{\nu}(T), \tag{4}$$

$$K = \frac{v_{max}}{k_1^+} = K_0 f_K(T),$$
(5)

$$f_R(T) = 1 - exp\left(-\frac{\Delta G_R}{RT}\right),\tag{6}$$

and  $v_{max,0}$  and  $K_0$  are values of  $v_{max}$  and K evaluated at temperature  $T_0$ , respectively.

For equation (6),  $f_R(T)$  can be computed following Jin and Bethke (2003), with  $\Delta G_R$  dependent on its reference value at standard conditions and the reaction quotient of the chemical reaction under the given environmental condition (characterized by pressure, temperature, salinity, pH, etc.). However, except when there is significant product inhibition,  $f_R$ may be set to one, which is adopted in the remainder of this paper. We next derive expressions for  $f_v(T)$ ,  $f_K(T)$  and  $f_E(T)$ .

For  $v_{max}$ , applying the transition state theory (Eyring, 1935), we have

$$f_{\nu}(T) = \left(\frac{T}{T_0}\right) exp\left(-\frac{\Delta H_V}{RT}\left(1 - \frac{T}{T_0}\right)\right),\tag{7}$$

115 where  $T_0$  is the reference temperature when  $v_{max}$  equals  $v_{max,0}$ , and  $\Delta H_V$  is the temperature-independent enthalpy of activation. In deriving equation (7), the Gibbs free energy  $\Delta G_V$  of transition state theory is taken as a linear function of temperature, i.e.  $\Delta G_V = \Delta H_V - T \Delta S_V$ , with entropy  $\Delta S_V$  being constant, and incorporated into  $v_{max,0}$ .

To derive the temperature dependence  $f_K(T)$  for K, we follow the definition of K in equation (2), and adopt the assumption that  $v_{max}$  is much greater than  $k_1^-$  in equation (5). Applying the diffusion-limited chemical reaction model by von Smoluchowski (1917) indicates that  $k_1^+$  is proportional to diffusivity. Therefore, by using the Stokes-Einstein equation of diffusivity (Miller, 1924), and considering the Arrhenius-type temperature dependence of water's dynamic viscosity,  $k_1^+$  will have a similar functional form of temperature dependence as  $v_{max}$  (see (Tang et al., 2021) for more details), resulting in

$$f_K(T) = exp\left(-\frac{\Delta H_K}{RT}\left(1 - \frac{T}{T_0}\right)\right).$$
(8)

In application, considering the activation enthalpy of self-diffusion of water as constant, e.g., 18 kJ mol<sup>-1</sup> (Konya and Nagy, 2018), one may compute  $\Delta H_K = \Delta H_V - 18$ .

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A two-state model (e.g., Zwanzig, 1997) is used to formulate the temperature dependent function  $f_E(T)$  as

$$f_E(T) = \frac{1}{1 + exp\left(-\frac{\Delta G_E}{RT}\right)},\tag{9}$$

with *R* being the universal gas constant, and protein-unfolding Gibbs free energy

$$\Delta G_E = \Delta H_E - T \Delta S_E = \Delta C_p (T - T_H) - T \Delta C_p ln \left(\frac{T}{T_s}\right).$$
(10)

Here  $\Delta C_p$  is the heat capacity of protein unfolding (computed as  $\partial \Delta H_E / \partial T = T \partial \Delta S_E / \partial T$ ), which is of opposite sign of the negative heat capacity of refolding measured by Oliveberg et al. (1995) and is always positive due to proteins' hydrophobicity (Silverstein, 2020).  $T_H$  is the temperature at which unfolding enthalpy  $\Delta H_E$  is zero, and  $T_S$  is the temperature at which unfolding entropy  $\Delta S_E$  is zero.  $\Delta C_p$ ,  $T_H$  and  $T_S$  are all functions of protein chain length (Ghosh and Dill, 2009), and, usually,

 $T_S$  is greater than  $T_H$ .

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When equations (3)-(8) are combined, we have

$$F = v_{max,0} \frac{f_{v}(T)f_{E}(T)E_{t}S}{K_{0}f_{K}(T)+S},$$
(11)

which describes the temperature dependence of biochemical reaction rates in the absence of significant product inhibition. When equation (11) is applied to represent the temperature dependence of an enzymatic reaction, once the reference temperature  $T_0$  is chosen, one needs to estimate four parameters:  $T_H$ ,  $T_S$ ,  $\Delta H_V$  and  $\Delta C_p$ .

In particular, by assuming that S is much larger than  $K_0 f_K(T)$ , we obtain the substrate unlimited rate equation

$$F_{\infty} = v_{max,0} E_t f_{\nu}(T) f_E(T) = r_0 f_{\nu}(T) f_E(T),$$
(12)

which is the four-parameter model proposed by Ratkowsky et al. (2005) to describe the temperature-dependent growth of various microorganisms (also see Corkrey et al., 2012; Corkrey et al., 2014). Since the Ratkowsky model has been successfully applied to hundreds of published datasets, the more generic chemical kinetics theory should be equally accurate under substrate-unlimited conditions, and can provide further insights to the non-monotonic relationship between enzymatic reaction rates, temperature, and substrate availability.

To facilitate parametric fitting (as will be described in section 2.3), taking the logarithm of equation (11) leads to

$$\ln F(T) = \ln v_{max,0} + \ln(1 + S/K_0) + \ln\left(\frac{f_v(T)f_E(T)}{f_K(T) + S/K_0}\right).$$
(13)

#### 2.3 Empirical data reanalysis

We extracted the assay data of all seven enzymes from Hobbs et al. (2013) and all five enzymes from Peterson et al. (2004) to evaluate the chemical kinetics theory. We did not try to analyze data from soils, as that would involve a more comprehensive model (considering both the production and destruction of enzymes), which is beyond the scope of this study. Since we were not able to extract the reaction rates directly from the figures in these studies, nor obtain the original data, rates for each enzyme were normalized with its own rate at a selected reference temperature  $T_r$ , based on the criterion that the data point at  $T_r$  is crossed by lines of their original numerical fitting ((Hobbs et al. (2013) used MMRT and Peterson et al. (2004)

- 150 used their equilibrium model). In the logarithm form (i.e.,  $\ln F(T)$ ), this normalization ensures that the values of  $\ln F(T) \ln F(T_r)$  used as observations at different temperatures are independent of the value of  $\ln v_{max,0} + \ln(1 + S/K_0)$  at the reference temperature  $T_0$  of the enzyme essay. We obtain the best-fit parameters by using the "fminsearch" function from MATLAB R2020b to minimize the summed difference between modeled and measured values of  $\ln F(T) \ln F(T_r)$ . In the process of parameter estimation, we found that "fminsearch" estimated the same parameter values corresponding to the global
- 155 minimum of the cost function even when starting from differential initial guesses, indicating that the parametric fitting is robust. However, this robustness leads to some difficulty in estimating the uncertainty of the parameter fitting process. Specifically, because we were not able to digitally extract meaningful uncertainty of the observations from the figures either in Peterson et al. (2004) or in Hobbs et al. (2013), we could not apply the Monte Carlo method to compute uncertainties of the estimated parameters. We also tried using finite difference to approximate the Hessian matrix of the cost function at the best
- 160 parameter estimates obtained by "fminsearch". However, the ill-condition of the approximated Hessian matrix prevents us from estimating the parametric uncertainty meaningfully. We could not apply the bootstrapping method because too few data points were available. Nonetheless, the excellent parametric fitting indicates that the results are robust.



Figure 2. Fitting of the chemical kinetics theory (solid lines) to the enzyme assay data (red filled circles). Panels (a)-(g) are measurements from Hobbs et al. (2013) and panels (h)-(l) are from Peterson et al. (2004).  $T_r$  is the reference temperature used in the data extracted from published figures (and is different from the reference temperature  $T_0$  that was actually involved in the enzyme assay experiments).  $R^2$  is for the linear regression between the model predictions with best-fit parameters (blue lines) and measurements (in red circles). Following their original studies, parametric fitting for panels (f) and (g) used  $S/K_0=2$ , while others used  $S/K_0=10$ .

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#### 3. Results

For the data of all twelve enzyme assays, the chemical kinetics theory obtained almost perfect model-data fitting with the "fminsearch" computed best fit parameters (Figure 2). The R<sup>2</sup> values for the linear regression between model predictions and observations are above 0.97 for 11 cases, and 0.85 for 1 case (Barnase) (Figure 2f). The best-fit heat capacity  $\Delta C_p$  of the

175 thermodynamically reversible conversion between active and inactive conformation states of the enzymes are all positive, varying between 1.34 kJ mol<sup>-1</sup> K<sup>-1</sup> (for Adenosine deaminase in Figure 2i) and 22.74 kJ mol<sup>-1</sup> K<sup>-1</sup> (for Aryl-acylamidase in Figure 2k), in agreement with the range reported in Figure 2C by Ghosh and Dill (2009).



Figure 3. Substrate availability strongly affects the temperature sensitivity of the enzymatic reaction rates, as shown for 4 example enzymes chosen from parameters inferred in Figure 2. For substrate level c4, the rate curve corresponds to  $f_v(T)f_E(T)$  from equation (12). The bulge in Figure 3d is due to the special combination of the inferred parameters.

For the four example enzymes chosen from the estimated parameters from Figure 2, we found the optimal temperature (i.e., where the reaction rate reaches its maximum) has varying dependence on substrate availability (Figure 3). We show temperature response curves of the other eight enzymes in Supplemental Material, and note that they show similar patterns as those in Figure 3. All examples show that as substrate availability increases, the optimal temperature increases and the temperature response curve shifts towards higher temperatures. For enzyme aryl-acylamidase (Figure 3d), the true physiological optimal temperature under the saturating substrate concentration (i.e., when  $S = \infty$ , computed by equation (12)) equals the emergent optimal temperature at a substrate concentration of  $10K_0$ , and is 1 K higher than those at substrate concentrations of  $K_0$  and  $K_0/2$ . For enzymes V200S and A43C/S80C, the optimal temperature at substrate concentration  $10K_0$ 

190 is 1 K lower than the physiological optimal temperature (Figure 3a, b). However, this difference is 20 K for adenosine deaminase (Figure 3c). These results clearly demonstrate that substrate availability plays a potentially important role in the emergent temperature response of biochemical reaction rates. Nevertheless, we note that this prediction of substrate

abundance-induced shift in optimal temperature is appropriate for single enzyme reactions. As we discuss below, the relationship between optimal temperature and substrate abundance in real soils is much more complicated.

#### 195 **4. Discussion and conclusion**

Our theoretical analysis suggests that, even for a single-substrate-single-enzyme reaction, its temperature response involves contributions from at least four processes: (1) the thermally reversible transition between active and inactive enzymes (which is ensured by the ceaseless thermal motions of molecules and ions in the enzyme solution); (2) the binding between active enzymes and substrates to form enzyme-substrate complexes; (3) the transition state activation of the enzyme-substrate

- 200 complex; and (4) the thermodynamic feasibility for the biochemical reaction to generate product molecules. The chemical kinetics theory explicitly accounts for these four processes, and can be extended to include more processes when more complex biochemical reactions are considered (e.g., as discussed in Tang et al. (2021)). In particular, this theory demonstrates that substrate availability affects the functional relationship between biochemical rates and temperature (equation (11)). Ignoring this effect may lead to misinterpretation of observed optimal temperatures, and confound analyses of, e.g., microbial thermal
- 205 adaptation. Specifically, we find that higher optimal temperatures can be achieved under higher substrate availability for a single-enzyme-single-substrate reactions. Such a shift in optimal temperature with substrate abundance also appears to align with the findings in Alvarez et al. (2018), although their interpretation attributes it to irreversible enzyme denaturation.



Figure 4. An example demonstrating that lower activation energy causes the optimal temperature to shift towards lower values. The curves are drawn based on equation (12), with the high activation energy case using parameters from V200S, and the low activation energy case reduced  $\Delta H_V$  from 78.82 kJ mol<sup>-1</sup> to 58.82 kJ mol<sup>-1</sup>.

Recently, Numa et al. (2021) and Robinson et al. (2020) observed that adding plant litter or glucose to soil incubation samples resulted in lower inferred optimal temperatures of soil respiration (when fitted with MMRT). Since adding more substrate most likely increased substrate concentrations, the lower optimal temperature appeared to contradict predictions by
the chemical kinetics theory. However, applying the chemical kinetics theory to soils requires consideration of interactions between substrates, microbes, and organo-mineral interactions. Since sorption interactions between organic matter and soil minerals tend to increase the overall activation energy or enthalpy of carbon use by microbes (Tang and Riley, 2015), and newly added substrates most likely have lower activation energy than existing soil organic substrates, we expect a decrease in the optimal temperature of soil respiration. We explore this effect by computing temperature response curves for low and high activation energy reduced the optimal temperature by ~2 K (Figure 4). Therefore, what Numa et al. (2021) and Robinson et al. (2020) observed could have resulted from a shift in substrate type and availability, which should be modelled through explicit representation of substrate competition and organo-mineral interactions (as discussed in (Tang and Riley, 2013;Tang

and Riley, 2015)). In particular, we argue that the change in optimal temperature is not a simple indication of microbial

225 physiological adaption, but an emergent consequence due to interactions among many factors, including substrate availability, soil conditions, enzyme dynamics, and among others, microbial physiology.

One important feature of the chemical kinetics theory is that it infers a positive heat capacity of protein unfolding (i.e.,  $\Delta C_p$  associated with thermally reversible enzyme denaturation), and a constant enthalpy of activation  $\Delta H_V$  of the forward conversion of the enzyme-substrate complex. This positive  $\Delta C_p$  is consistent with the negative heat capacity of enzyme 230 refolding found by Oliveberg et al. (1995) and with many previous studies (Ghosh and Dill, 2009; Murphy et al., 1990; Finkelstein and Ptitsyn, 2016). Recently, using molecular dynamics simulations, Aqvist and Van der Ent (2022) inferred the heat capacity to be zero for both catalysis and binding processes for a designer enzyme 1A53-2.5, supporting a constant  $\Delta H_V$ (note that heat capacity equals to  $\partial H_V/\partial T$ ). Moreover, Aqvist and Van der Ent (2022) and Aqvist (2022) suggested that the non-monotonic relationship between temperature and catalysis rate can be explained by the existence of an equilibrium between active enzyme substrate complex  $E_nS$  and inactive enzyme substrate complex  $(E'_nS)$ . To some extent, the conceptual 235 model by Aqvist and Van der Ent (2022) is equivalent to the chemical kinetics theory, if the latter allows the inactive enzymes to form inactive enzyme-substrate complexes. The finding of zero heat capacity for both catalysis and binding processes has been debated in Lear et al. (2023) and Aqvist (2023), but they concluded that different kinetic models can fit the measured temperature dependent catalysis rates equally well. In particular, Aqvist (2023) noted that a kinetic model considering 240 thermally reversible enzyme denaturation fits the observations equally well. However, deducing a non-zero heat capacity for both catalysis and binding processes seems to require one to ignore the thermally-reversible enzyme denaturation, which is inconsistent with the ceaseless thermal motion of molecules and ions in the enzyme solution.

Combining the transition state theory and the protein denaturation model by Lumry and Eyring (1954), Peterson et al. (2004) proposed an equilibrium model that includes both reversible and irreversible enzyme denaturation to explain their observed non-monotonic relationship between temperature and catalysis rates. However, because they assumed a constant enthalpy for the reversible enzyme denaturation, their Gibbs free energy of enzyme unfolding became a linear function of temperature. This linear function contrasts with the nonlinear function (i.e. equation (10)) and the existence of multiple native protein states that are usually observed or inferred in studies of protein physics (Ghosh and Dill, 2009; Silverstein, 2020; Sheng and Pan, 2002; Finkelstein and Ptitsyn, 2016). Further, their model involves an explicit temporal dependence in the formulated

250 catalysis rates, which introduces one more parameter (i.e., time) than the chemical kinetics model. Moreover, Peterson et al. (2004) also assumed their enzyme essays are substrate saturated, which is not always the case in real systems, and can affect the temperature dependence of the substrate affinity parameter and thereby the overall reaction rate.

In summary, we show here that the chemical kinetics theory, by incorporating (1) the observed thermally reversible transitions of enzymes between their active and inactive states (which occurs even in the absence of substrate molecules due to the ceaseless thermal motion of molecules and ions in the enzyme solution) (Anfinsen, 1973; Finkelstein and Ptitsyn, 2016; Sizer, 1943; Oliveberg et al., 1995); (2) law of mass action (Koudriavtsev, 2011); (3) the diffusion-limited chemical reaction theory by von Smoluchowski (1917); and (4) the transition state theory by (Eyring, 1935), can satisfactorily explain the non-

- monotonic relationship between temperature and catalysis rates, and is a more comprehensive mechanistic representation of the temperature dependence of enzyme-catalyzed biochemical rates.
- Can chemical kinetics theory be upscaled to an organism from the single-substrate-single-enzyme examples presented here? While it is likely impossible (and certainly beyond the scope of this paper) to demonstrate such a scaling analytically, Tang et al. (2021) showed, with an Ohm's law analogy, that the temperature dependence of the emergent kinetic parameters (i.e., the overall  $v_{max}$  and K) for chains of enzymes followed a similar form as described by the chemical kinetics theory. Indeed, some previous studies (e.g., Ratkowsky et al., 2005; Corkrey et al., 2012; Ghosh et al., 2016) have showed that even equation (12) (which excludes substrate dependence) is able to satisfactorily describe temperature dependent growth of many organisms. Particularly, the success in capturing the temperature-dependent bacterial growth rate in Ghosh et al. (2016), where they extended the thermally reversible enzyme denaturation in equation (12) to include all lethal proteins sampled from the proteome of mesophilic and thermophilic bacteria, suggests that the chemical kinetics theory may be scalable to organisms. Further work is required to evaluate whether the chemical kinetics theory has the potential to be applied directly to microbes,

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animals, and plants.
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Finally, because almost every microbe, animal, and plant is able to respire on multiple substrates (Madigan et al., 2009; Cooper and Hausman, 2007) and the availability of those substrates fluctuates at multiple time scales, the chemical kinetics theory and the equilibrium chemistry approximation kinetics for substrate competition networks (Tang and Riley,

2013) together suggest that a given organism will be unlikely to have either a fixed temperature response curve or optimal

275 temperature even with a fixed proteome distributions. Rather, the temperature response curve, and therefore the optimal temperature, is likely to be dynamic, motivating inclusion of these concepts in biogeochemical models.

# Appendix

# Nomenclature

Symbol	Unit	Meaning
$\Delta C_p$	kJ mol <sup>-1</sup> K <sup>-1</sup>	Heat capacity of protein unfolding.
$\Delta G_R$	kJ mol <sup>-1</sup>	Gibbs free energy of the chemical reaction.
$\Delta G_E$	kJ mol <sup>-1</sup>	Gibbs free energy of protein unfolding.
$\Delta H_K$	kJ mol <sup>-1</sup>	Enthalpy of activation of parameter K.
$\Delta H_{v}$	kJ mol <sup>-1</sup>	Enthalpy of activation of $v_{max}$ .
$\Delta H_E$	kJ mol <sup>-1</sup>	Enthalpy of protein unfolding.
$\Delta S_E$	kJ mol <sup>-1</sup>	Entropy of protein unfolding
С	mol m <sup>-3</sup>	Enzyme-substrate complex concentration.
$E_n$	mol m <sup>-3</sup>	Free active enzyme concentration.
$E_{nt}$	mol m <sup>-3</sup>	Total active enzyme concentration.
$E_t$	mol m <sup>-3</sup>	Total enzyme concentration.
F	mol m <sup>-3</sup> s <sup>-1</sup>	Biochemical reaction rates.
$F_{\infty}$	mol m <sup>-3</sup> s <sup>-1</sup>	Biochemical reaction rates when substrate is unlimited.
<i>K</i> <sub>0</sub>	mol m <sup>-3</sup>	Half saturation parameter at reference temperature $T_0$ .

Κ	mol m <sup>-3</sup>	Half saturation parameter at temperature <i>T</i> .
Р	mol m <sup>-3</sup>	Product concentration.
R	J K <sup>-1</sup>	Universal gas constant.
S	mol m <sup>-3</sup>	Free substrate concentration.
Т	K	Thermodynamic temperature.
$T_H$	K	Temperature when $\Delta H_E$ is zero.
$T_S$	K	Temperature when $\Delta S_E$ is zero.
$f_K(T)$	None	Temperature dependence of parameter <i>K</i> .
$f_R(T)$	None	Thermodynamic potential of the chemical reaction at $T$ .
$f_v(T)$	None	Temperature dependence of $v_{max}$ .
$k_1^+$	m <sup>3</sup> mol <sup>-1</sup> s <sup>-1</sup>	Specific forward binding rate between active enzymes and substrates.
$k_1^-$	s <sup>-1</sup>	Specific enzyme-substrate complex dissociation rate.
$r_0$	mol m <sup>-3</sup> s <sup>-1</sup>	Biochemical reaction rate at temperature $T_0$ .
$v_{max,0}$	s <sup>-1</sup>	Maximum specific catalysis rate at reference temperature $T_0$ .
$v_{max}$	s <sup>-1</sup>	Maximum specific catalysis rate at reference temperature <i>T</i> .

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